

## INTRODUCTION AND AIM OF THE WORK

The need to improve fertilizer use efficiency (FUE) is one of the major challenges for modern agriculture and environmental sustainability. Animal manures, especially in liquid form, represent very important organic fertilizers but their very high availability of nutrients, especially in the form of  $\text{NH}_4^+$ , stimulates soil microbial activity leading to rapid N transformations and significant losses from the soil in the form of  $\text{NO}_3^-$  and N GHG gasses, causing severe environmental pollution. A valid methodology for contrasting this phenomenon is the use of (zeolites, ZEO), particular rocks with high zeolite content (>50%) in the treatment of zootechnical liquid manure (ZLM). These rocks are particularly efficient as sorbent of cationic species and hence their use can lead to a significant reductions of  $\text{NH}_4^+$  concentration. Then, once «charged» of  $\text{NH}_4^+$ , ZEO can be applied as soil amendments and act as slow release fertilizer.

While ZEO  $\text{NH}_4^+$  sorption from synthetic solutions is a well investigated field, actually there is a lack of knowledge regarding his sorption behavior in **real ZLM**.

The aim of this work is to deeply characterize  $\text{NH}_4^+$  adsorption by a chabazite-rich ZEO (CHA) quarried in center Italy, in contact with ZLM, in particular with swine manure. A series of batch experiments were conducted in order to define the equilibrium isotherms, kinetic models and thermodynamic parameters.

## MATERIALS

CHA

2 grain size selected

- Granular (0.7–2.0 mm), CHAg
- $\mu$ -sized (< 20  $\mu\text{m}$ ), CHA $\mu$

Both dried at 105 °C

SM\*

centrifuged at 4000 rpm for 8 min.

- Centrifuged swine manure, CSM

\* Initial pH = 8.07  
Initial  $\text{NH}_4^+$  = 3140  $\text{mg L}^{-1}$

## EXPERIMENTAL SETUP AND CALCULATIONS

### ISOTHERMS

- Batch experiments with different masses of CHA mixed with CSM for 20 h.
- pH barely varied during the experiment thus no pH correction was conducted.
- Air stripping evaluated by performing blanks.

TEMPERATURES	BEST MODELS	LINEAR EQUATIONS
13, 20, 37 °C	Harkins-Jura	$\frac{1}{q_e^2} = \beta \ln(C_e) + \alpha$
CHA DOSAGES	Freunlich	$q_e = K_F \times C_e^{1/n}$
0.5, 1, 3, 5, 8, 12 g	Langmuir	$\frac{1}{q_e} = \frac{1}{q_{\max} K_L} \frac{1}{C_e} + \frac{1}{q_{\max}}$

### KINETICS

- Batch experiments with a specific mass of CHA mixed with CSM based on CSM initial  $\text{NH}_4^+$  content.
- Only data sufficiently far from equilibrium were considered:  
 $F(t) < 85\%$ ,  $F(t) = q(t)/q_e$
- Temperature fixed at 20 °C.
- The experiments were conducted in 3 replicates.

BEST MODELS	LINEAR EQUATIONS
Pseudo-Second Order	$\frac{t}{q_t} = \frac{1}{q_e} t + \frac{1}{h}$
Intraparticle Diffusion	$q_t = K_{ID} t^{0.5} + C$
Elovich	$q_t = \frac{2.3}{\alpha} \ln(t + t_0) - \frac{2.3}{\alpha} \ln(t_0)$

## THERMODYNAMICS

METHODS APPLIED	LINEAR EQUATIONS
van't Hoff equation	$\ln(K_{eq}) = -\frac{\Delta H}{R} \frac{1}{T} + \frac{\Delta S}{R}$
Gibbs-Helmholtz	$\Delta G = \Delta H - T\Delta S$

- $\text{NH}_4^+$  were measured with an Ion Selective Electrode (ISE) Orion 95-12 connected to an Orion 4star pH-ISE benchtop (Thermo Fisher).

### Mathematical symbols in order of appearance

$q_e$ : equilibrium adsorption capacity ( $\text{mg g}^{-1}$ )	$K_{ID}$ : Intraparticle diffusion constant
$C_e$ : equilibrium concentration ( $\text{mg L}^{-1}$ )	C: intercept (graph $q_t$ vs. $t^{0.5}$ )
$\alpha, \beta$ : Harkins-Jura constants	$\alpha$ : initial adsorption rate constant
$K_F$ : Freundlich constant	$K_{eq}$ : equilibrium constant
$K_L$ : Langmuir constant	$\Delta H$ : free enthalpy change ( $\text{J mol}^{-1}$ )
$q_{\max}$ : maximum adsorption capacity ( $\text{mg g}^{-1}$ )	$\Delta S$ : free entropy change ( $\text{J K}^{-1} \text{mol}^{-1}$ )
$q_t$ : adsorption capacity at time t ( $\text{mg g}^{-1}$ )	$\Delta G$ : Gibbs free energy change ( $\text{kJ mol}^{-1}$ )
h: initial adsorption rate ( $\text{mg g}^{-1} \text{min}^{-1}$ )	T: Temperature (K)
t: time (min)	R: Universal gas constant ( $\text{J K}^{-1} \text{mol}^{-1}$ )

## RESULTS AND DISCUSSIONS

### ISOTHERMS

CHA $\mu$  and CHAg showed L3 type curve (Fig.1), thus the formation of a multilayer bonding structure occurred. There was no significative differences with respect to the temperatures tested for CHA $\mu$ , while temperatures has more relevant effects on CHAg.

Harkins-Jura was found to be the best isothermal model (Fig.2).

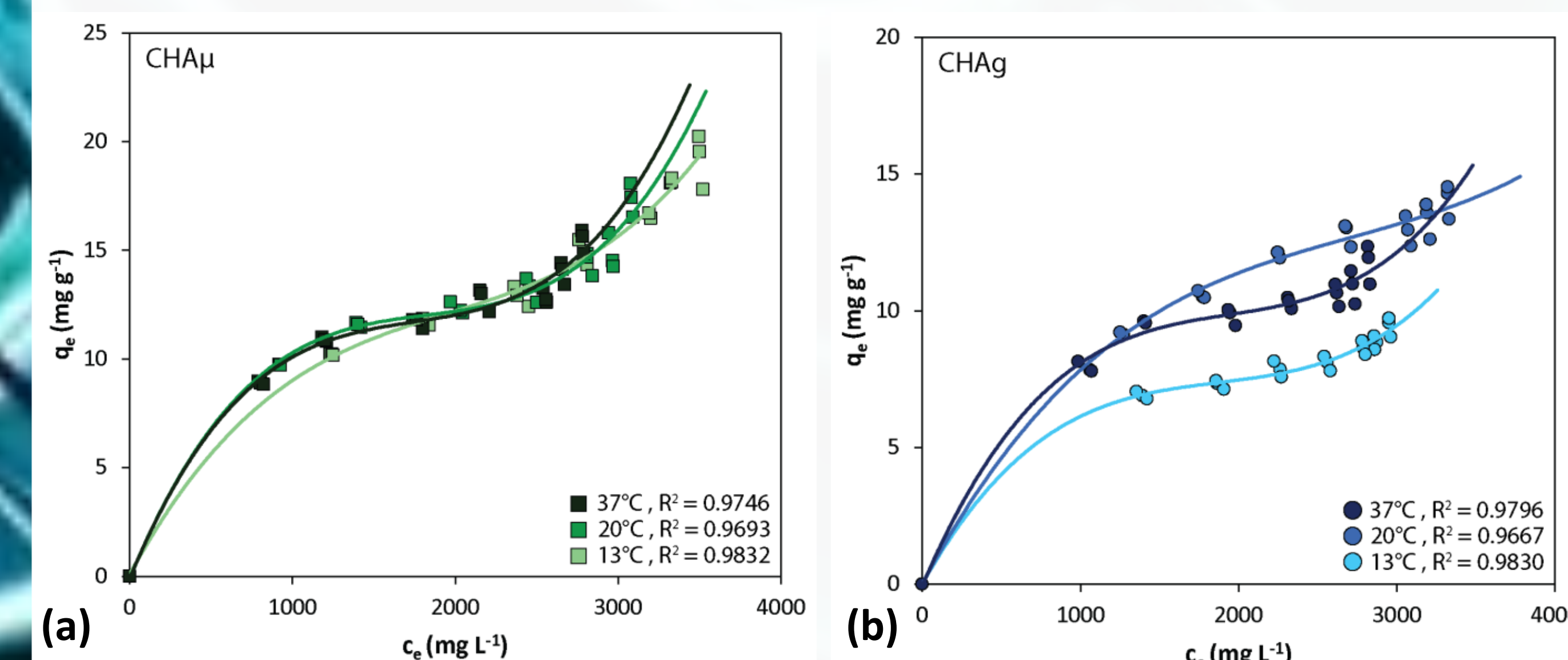


Figure 1.  $C_e$  against  $q_e$  curves and relative  $R^2$ . (a) CHA $\mu$ , (b) CHAg

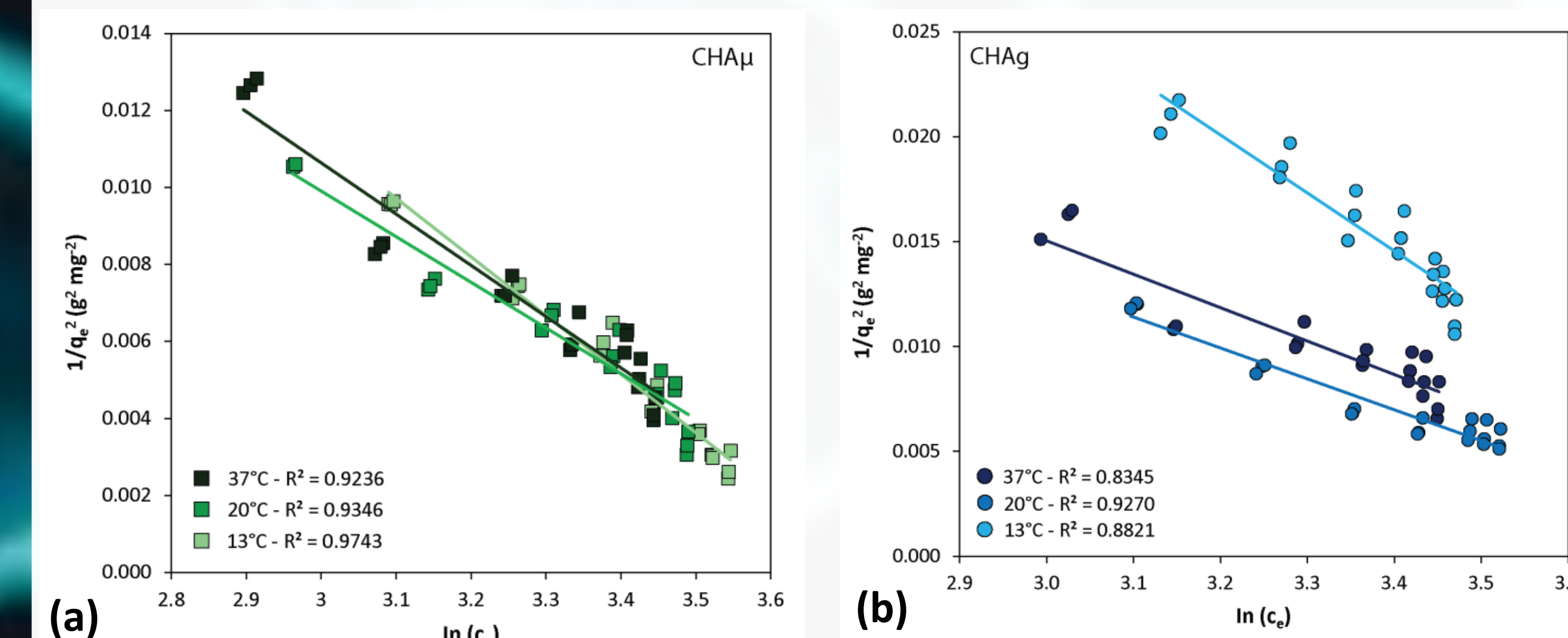


Figure 2. Harkins-Jura isotherms and relative  $R^2$ . (a) CHA $\mu$ , (b) CHAg

### KINETICS

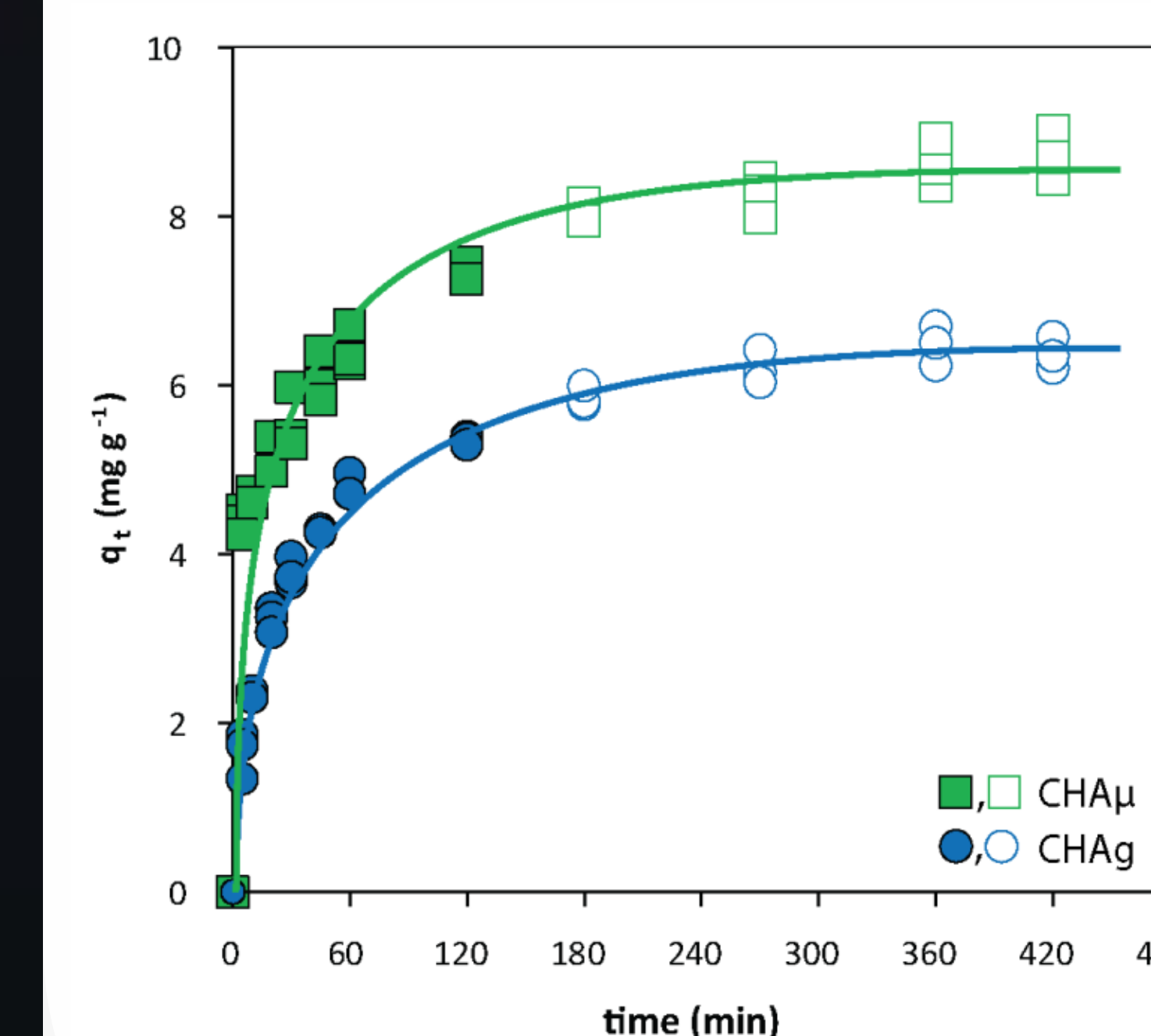


Figure 3.  $q_t$  against t, empty dots are data not considered in kinetic analysis ( $F(t) > 85\%$ ).

$\text{NH}_4^+$  sorption for CHA $\mu$  and CHAg has shown differences in the sorption kinetics (Fig.3), in particular CHA $\mu$  adsorbed  $\text{NH}_4^+$  more rapidly than CHAg and reaches higher equilibrium capacity.

In the case of CHAg (Fig.4a) diffusion through macro and mesopores was the main process during the first 60 minutes of contact. During this phase a thin  $\text{NH}_4^+$  boundary layer were developed (thickness is proportional to the intercept C). After 1 hour the layer thickens significantly while  $\text{NH}_4^+$  slowly penetrates inside the micropores.

For CHA $\mu$  diffusion is not so important as for CHAg, as demonstrated by the high value of the intercept, and just within the first minutes of contact CHA $\mu$  has developed an adsorption layer thicker than CHAg (Fig.4b).

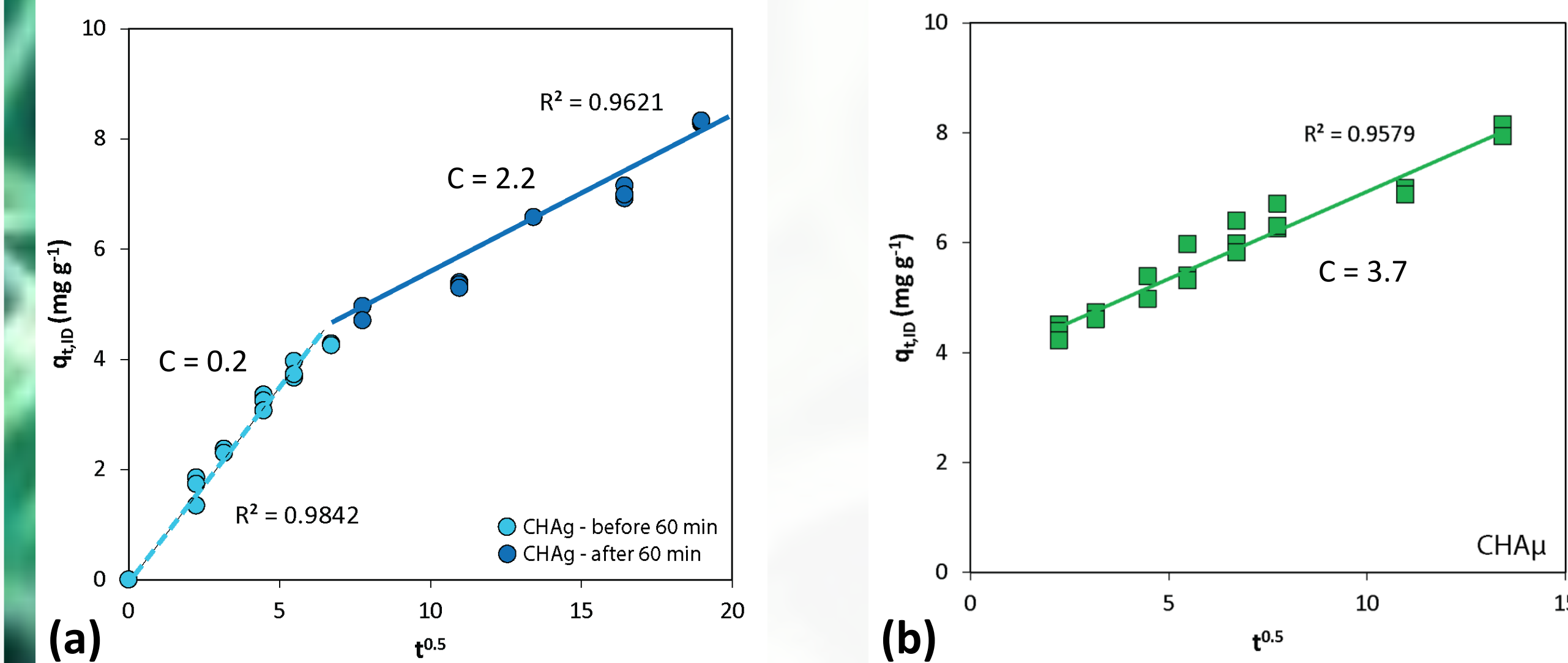


Figure 4. ID plots with  $R^2$  and intercept C values. (a) CHAg, (b) CHA $\mu$ .

## THERMODYNAMICS

Average values for 13, 20 and 37 °C

ZEO size	$\Delta H$ ( $\text{J mol}^{-1}$ )	$\Delta S$ ( $\text{J K}^{-1} \text{mol}^{-1}$ )	$\Delta G$ ( $\text{kJ mol}^{-1}$ )
CHAg	2492	12.5	-1.2
CHA $\mu$	2120	13.7	-1.9

The adsorption was endothermic and spontaneous ( $\Delta H > 0$ ,  $\Delta G < 0$ ) and it was associated with an increase of the randomness in the interphase between the solid and the liquid phase ( $\Delta S > 0$ ).

## CONCLUSIONS

In order to develop multilayer conditions and achieve maximum adsorption capacity ZEO should be applied at dosages < 6%. CHAg has performed better at higher temperatures. Kinetic analysis showed that CHA $\mu$  approaches equilibrium faster than the granular one and intraparticle diffusion was a relevant process for both.

The studied Italian chabazite-zeolite was confirmed as a valid material for the treatment of zootechnical liquid manure and these data can be of high value for future applications at field scale.